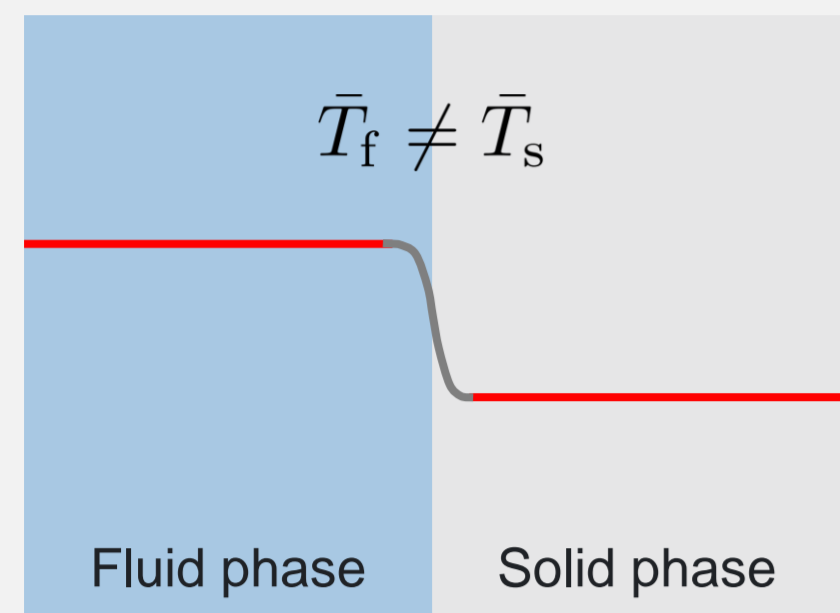


# Influence of Local Thermal Non-Equilibrium (LTNE) Processes in Saturated Porous Media and Coupled Systems

Anna Mareike Kosteletzky<sup>1</sup>, Maziar Veyskarami<sup>1</sup>, Rainer Helmig<sup>1</sup>  
<sup>1</sup>Institute for Modelling Hydraulic and Environmental Systems (IWS), University of Stuttgart

## Motivation

### What is LTNE?



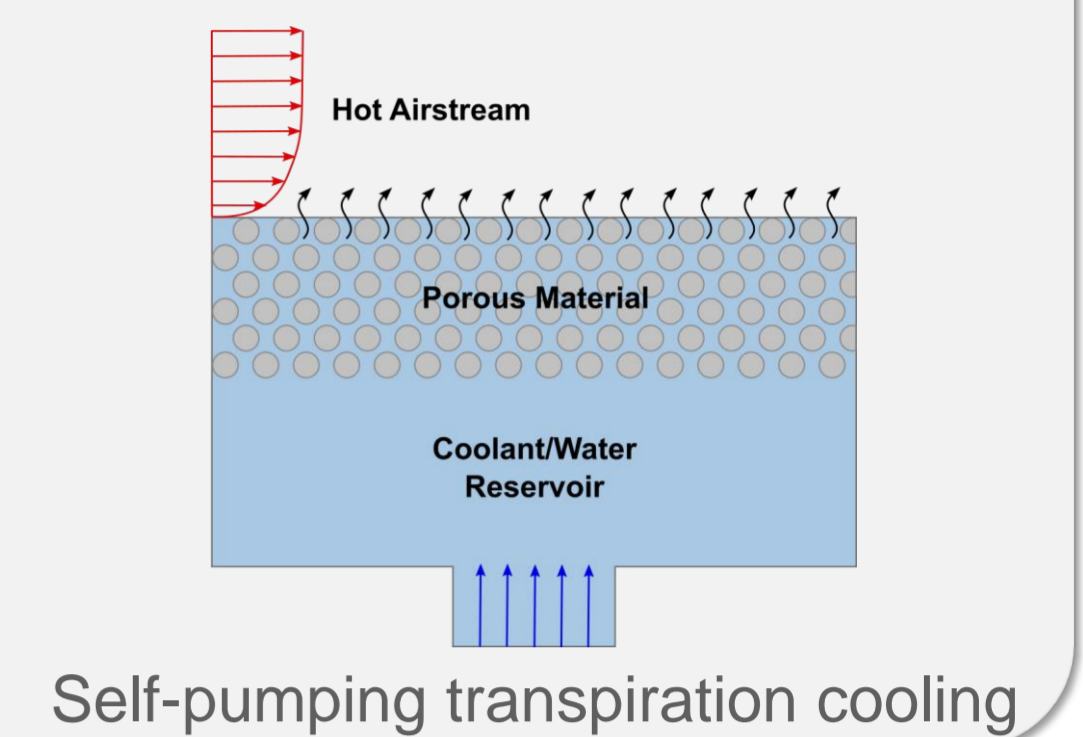
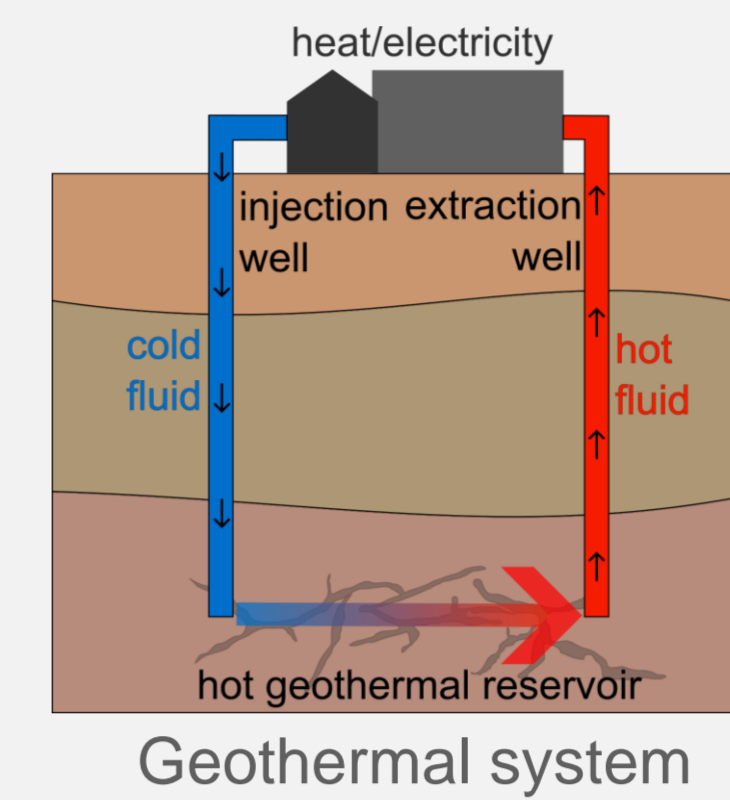
- No instantaneous heat transfer
- Different temperatures for different phases

### Why LTNE?

Assumption of instantaneous heat transfer not always applicable

Investigate LTNE processes in porous-medium and coupled free-flow systems across pore and REV scales.

### Applications



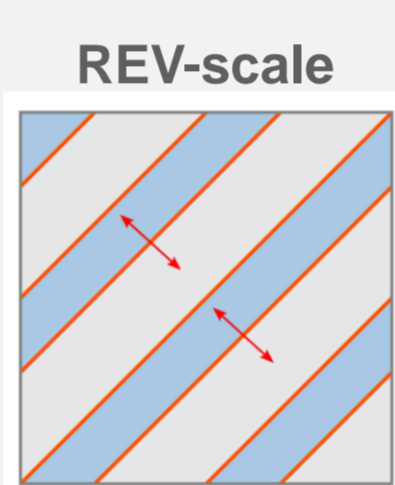
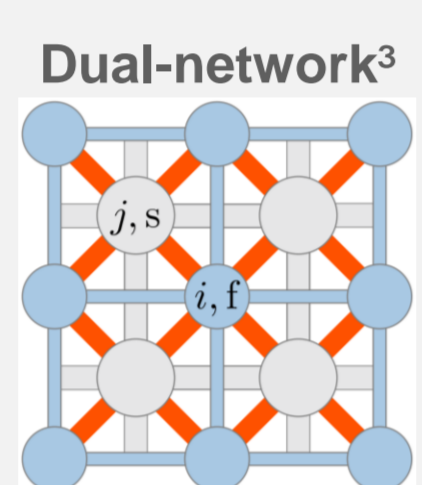
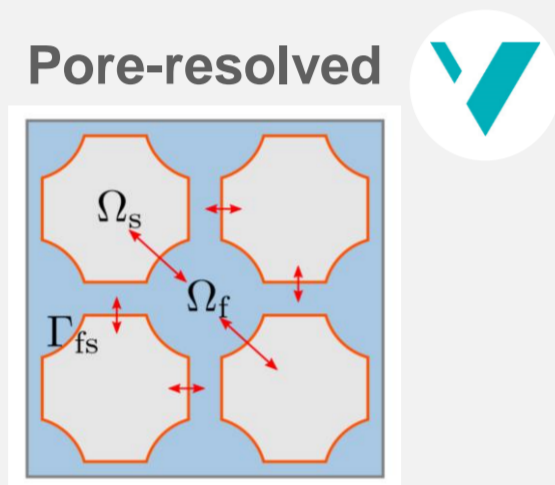
## Model Comparison<sup>1,2</sup>

### Study objective

- Systematic comparisons of LTNE models remain limited
- Evaluate consistency between & influence of different models

### Models

- Saturated porous medium



Flux continuity & T-jump

$$\lambda_f \nabla T_f \cdot \mathbf{n} = \lambda_s \nabla T_s \cdot \mathbf{n}$$

$$\lambda_f \nabla T_f \cdot \mathbf{n} = h(T_s - T_f)$$

Energy exchange term

$$Q_{i,f \rightarrow j,s} = t_{i,f \rightarrow j,s} (T_{i,f} - T_{j,s})$$

$$t_{i,f \rightarrow j,s} (\lambda_f, \lambda_s, A, h)$$

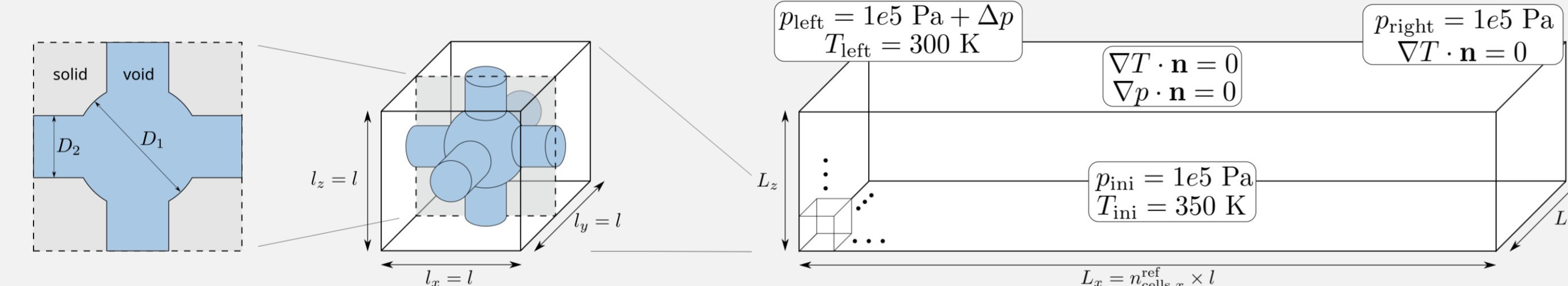
Energy exchange term

$$q_{cond,s \rightarrow f} = \lambda_{eff} a_{fs} (\bar{T}_s - \bar{T}_f)$$

→ Effective parameters needed  
 (λ<sub>f</sub><sup>eff</sup>, λ<sub>s</sub><sup>eff</sup>, λ<sub>f</sub>a<sub>fs</sub>, ...)  
 e.g. Homogenization, Nuske<sup>5</sup>, Nakayama<sup>4</sup>, ...

### Setup

- Cooling of a warmer, porous channel (isotropic, homogeneous)



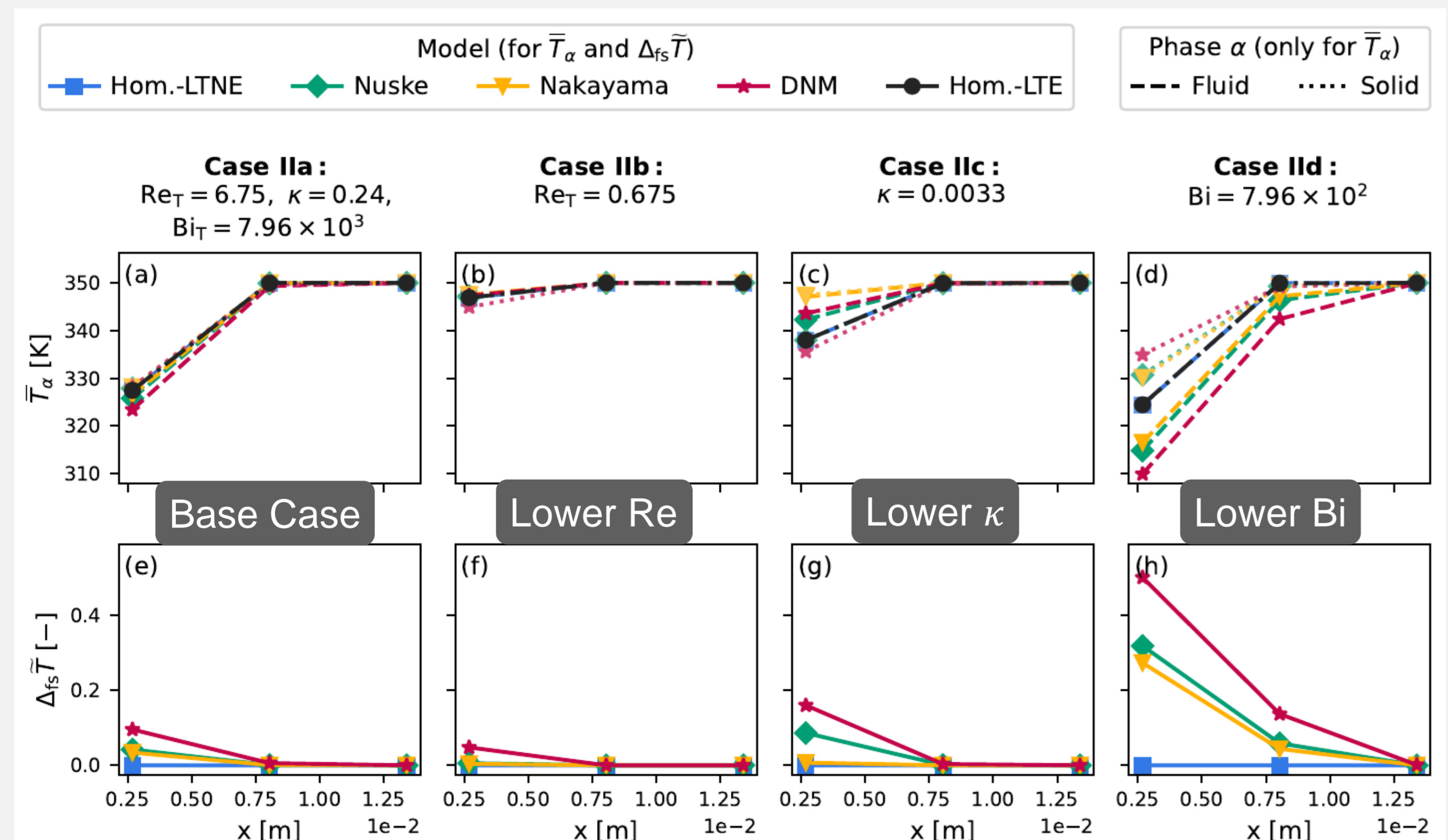
Cut-through of reference cell

Reference cell

Domain with initial and boundary conditions (45x4x4 reference cells)

### Results

- REV-scale temperatures (averaged for 15x4x4 ref. cells):  $\bar{T}_\alpha$
- Non-dimensional temperature difference:  $\Delta_{fs} \tilde{T} = \frac{\bar{T}_f - \bar{T}_s}{T_{left,f} - T_{ini,f}}$
- Investigation in terms of different non-dimensional numbers:  
 $Re_T = \frac{v_{x,T} L_T}{\nu_f}$ ,  $\kappa = \frac{\lambda_f}{\lambda_s}$ ,  $Bi_T = \frac{h L_T^2 a_{fs}}{\lambda_f}$



→ Differences in LTNE due to different orders of exchange term  
 → Larger LTNE for higher Re & lower Bi number

## Coupled Free-Flow Porous-Medium

### Energy coupling conditions (dual network – free flow)

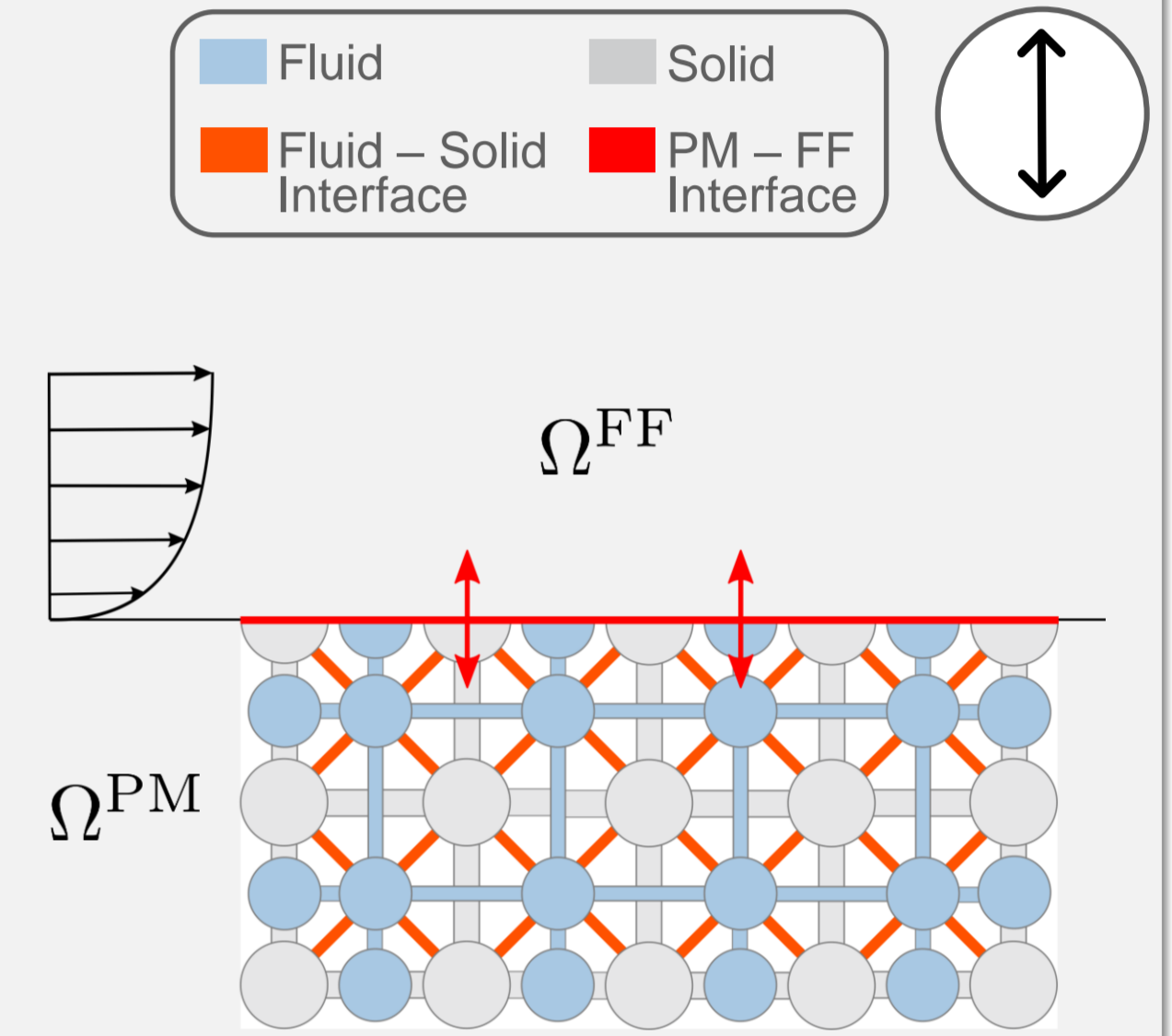
- Flux & Temperature continuity

$$T^{FF} = T^{PM,p}$$

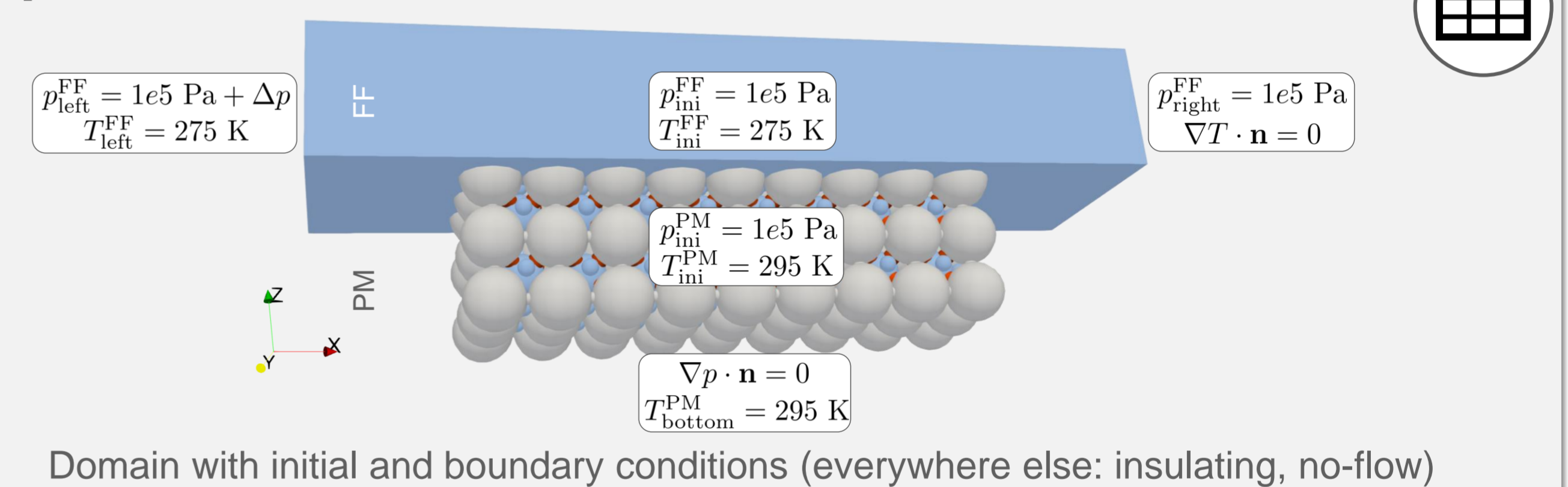
$$q_{cond.}^{FF} + conv. = q_{cond.}^{PM,p} + conv.$$

$$T^{FF} = T^{PM,s}$$

$$q_{cond.}^{FF} = q_{cond.}^{PM,s}$$

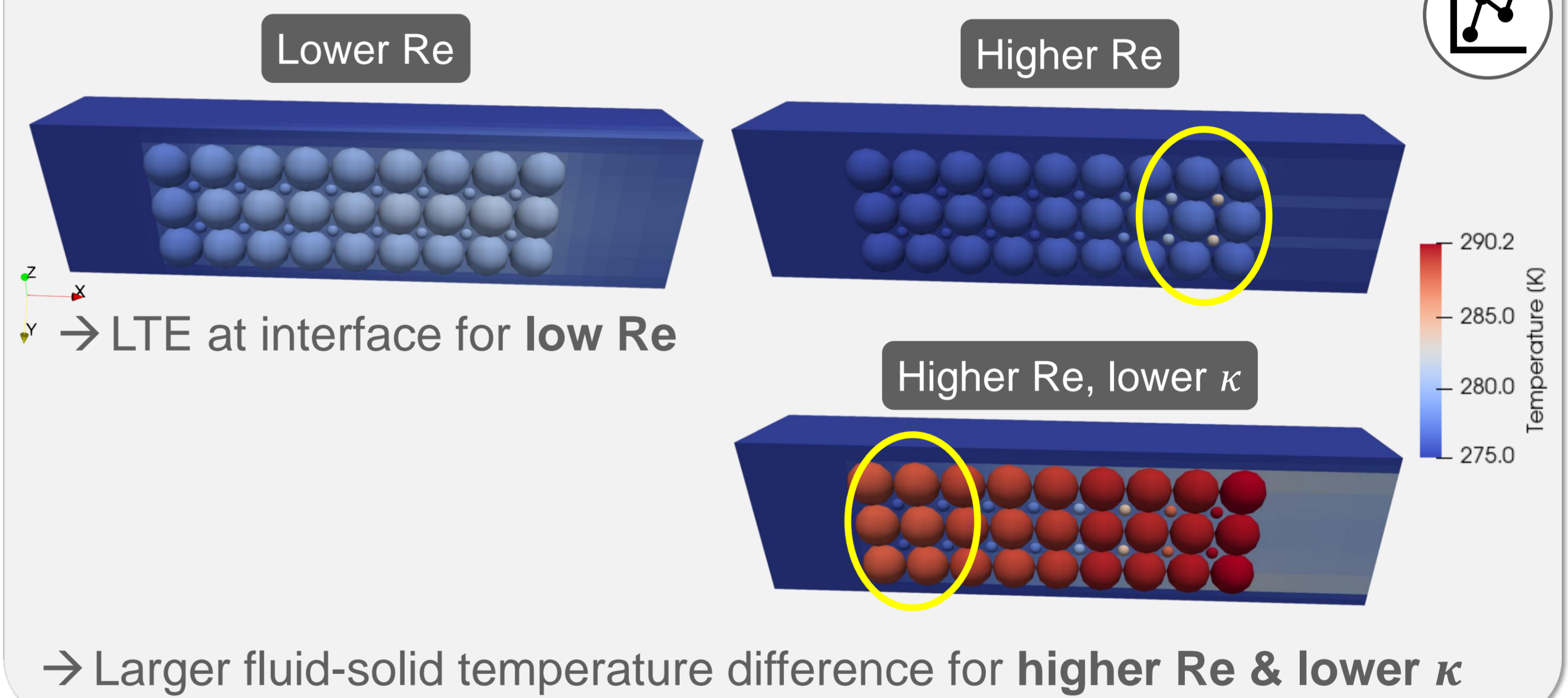


### Setup



Domain with initial and boundary conditions (everywhere else: insulating, no-flow)

### Results



→ Larger fluid-solid temperature difference for higher Re & lower κ

## Conclusion & Outlook

- LTE holds for conditions in natural porous media (low Re, moderate conductivity ratios, high Bi)
- LTNE becomes more relevant for larger Re & lower Bi
- Results are model dependent → **Benchmark studies needed**
- LTNE likely to occur at FF-PM interface for high Re & low κ
- Coupled dual network – free flow model:**  
 → Including temperature jump at FF – PM interface
- Extending dual-network model for **multi-phase flow**

## References

<sup>1</sup> Kosteletzky, A. M. et al. *Comparison study for Local Thermal Non-Equilibrium [...] model concepts [...]*. TiPM, 2026.  
<sup>2</sup> Kosteletzky, A. M. et al. *Comparison study [...]: Investigation of convection including conduction*. TiPM, submitted.  
<sup>3</sup> Koch, T. et al. *A (dual) network model for heat transfer in porous media, [...]*. Transport in porous media, 2021  
<sup>4</sup> Nuske, P. et al. *Modeling two-phase flow [...] with local thermal non-equilibrium on the Darcy scale*. IJHMT, 2015  
<sup>5</sup> Nakayama, A. et al., *A two-energy equation model for conduction and convection in porous media*, IJHMT, 2001

