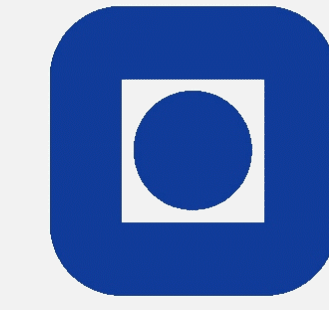


# How does the power law dependency of flow rate on pressure gradient when viscous and capillary forces compete, scale with system size?

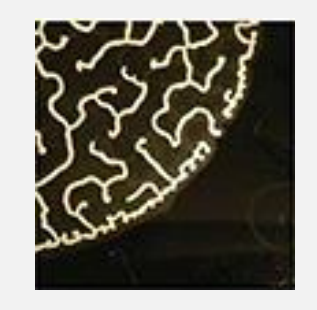
Subhadeep Roy<sup>a</sup>, Santanu Sinha<sup>a,b</sup> & Alex Hansen<sup>a</sup>

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NTNU



PoreLab



CSRC

## A. Introduction

**Immiscible 2-phase Flow:** When two immiscible fluids flow together through a porous media and both of them are fighting for the same pore space.

### Controlling Parameters

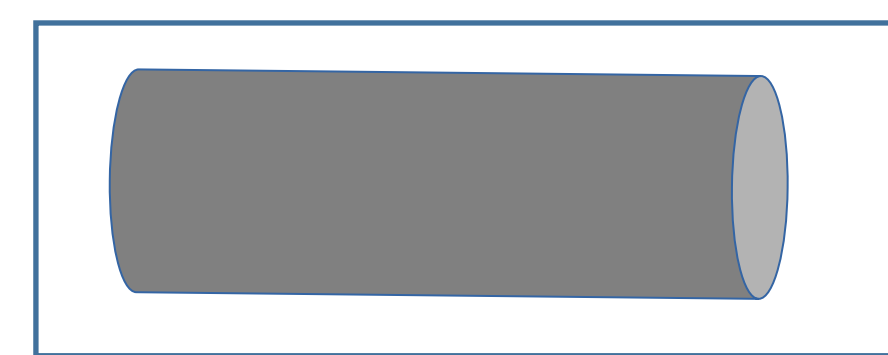
- Pressure gradient
- Geometry of the system
- Saturation of the fluids
- Capillary number  $Ca = \frac{Q\mu}{\gamma A}$
- Viscosity ratio

### Area of Application

Oil recovery, CO<sub>2</sub> sequestration, transport in fuel cells, ground-water management, catalyst support in automotive industry, blood flow in capillary vessels.

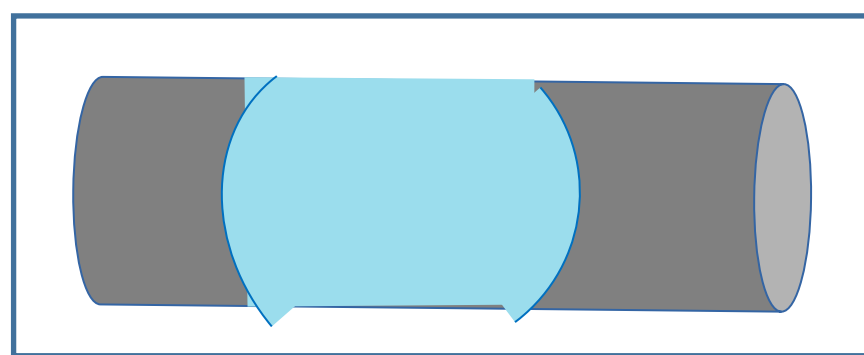
## Rheological Behavior

$$p_a \xrightarrow{q} p_b \quad \Delta p = p_a - p_b$$



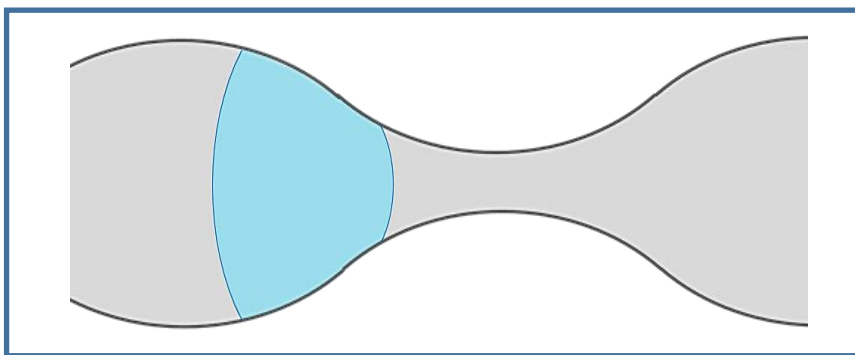
$$q = -\frac{\kappa A (p_b - p_a)}{\mu l}$$

Henry Darcy, Les Fontaines Publiques de la Ville de Dijon, Dalmont, Paris, 647 (1856)



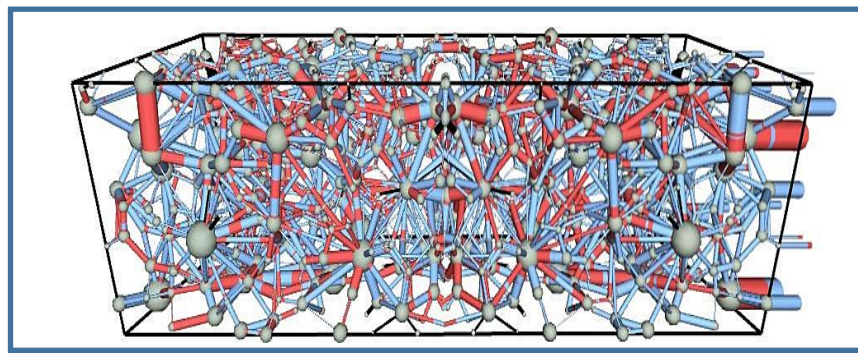
$$q = -\frac{\pi r^4}{8l\mu} \left( p_b - p_a - \sum p_c \right)$$

E. W. Washburn, *The dynamics of capillary flow*, Phys. Rev. 17, 273 (1921)



$$\langle q \rangle \sim \sqrt{\Delta p^2 - p_t^2}$$

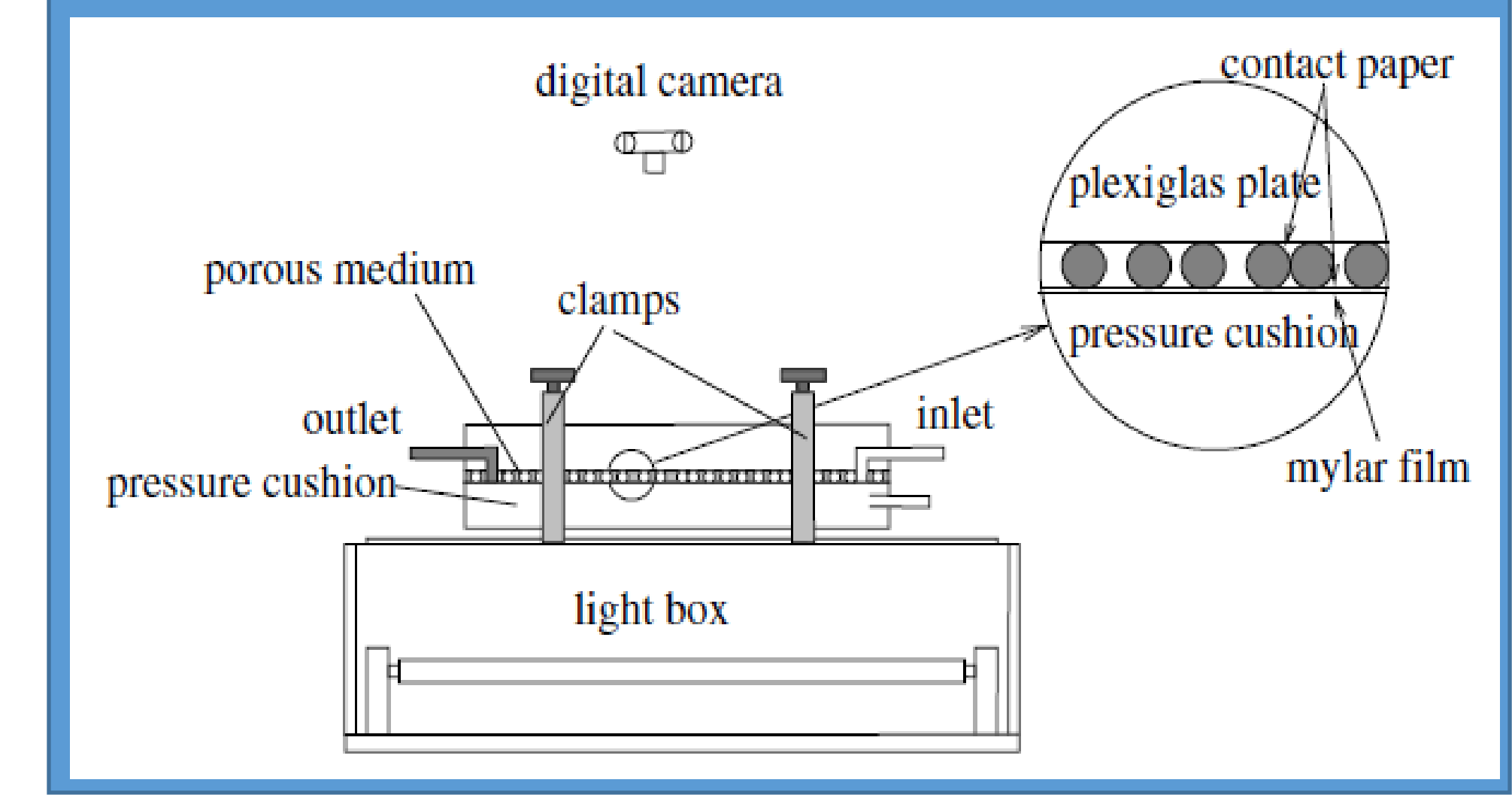
S. Sinha, A. Hansen, D. Bedeaux and S. Kjelstrup, Phys. Rev. E 87, 025001 (2013)



$$Q \sim \begin{cases} (|\Delta P| - P_t)^2, & |\Delta P| > \Delta P_c \\ 0, & |\Delta P| \leq \Delta P_c \end{cases}$$

Europhys. Lett. 99, 44004 (2012), Transp. Porous Med. 119, 77 (2017)

## B. Experiments [1,2,3]

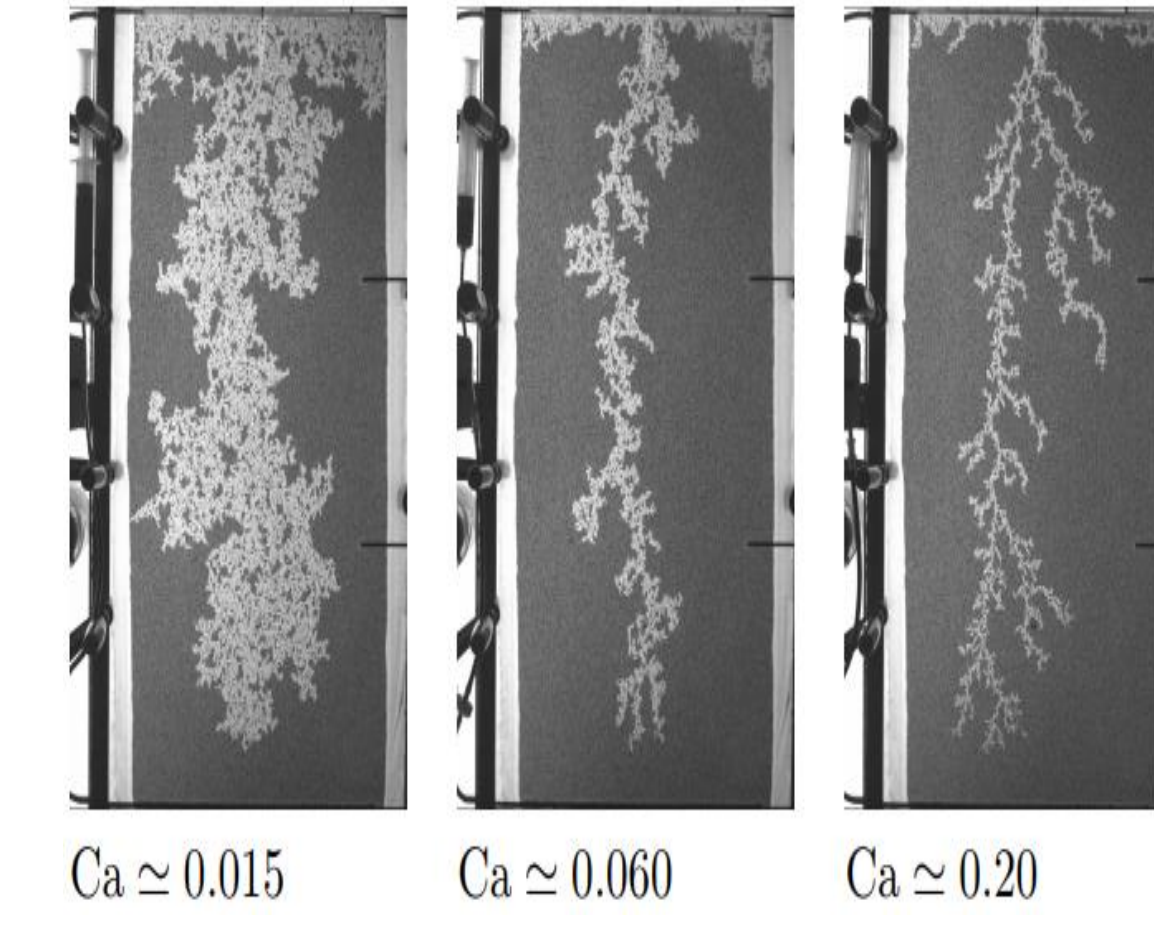


$$\Delta P \sim Ca^{0.54}$$

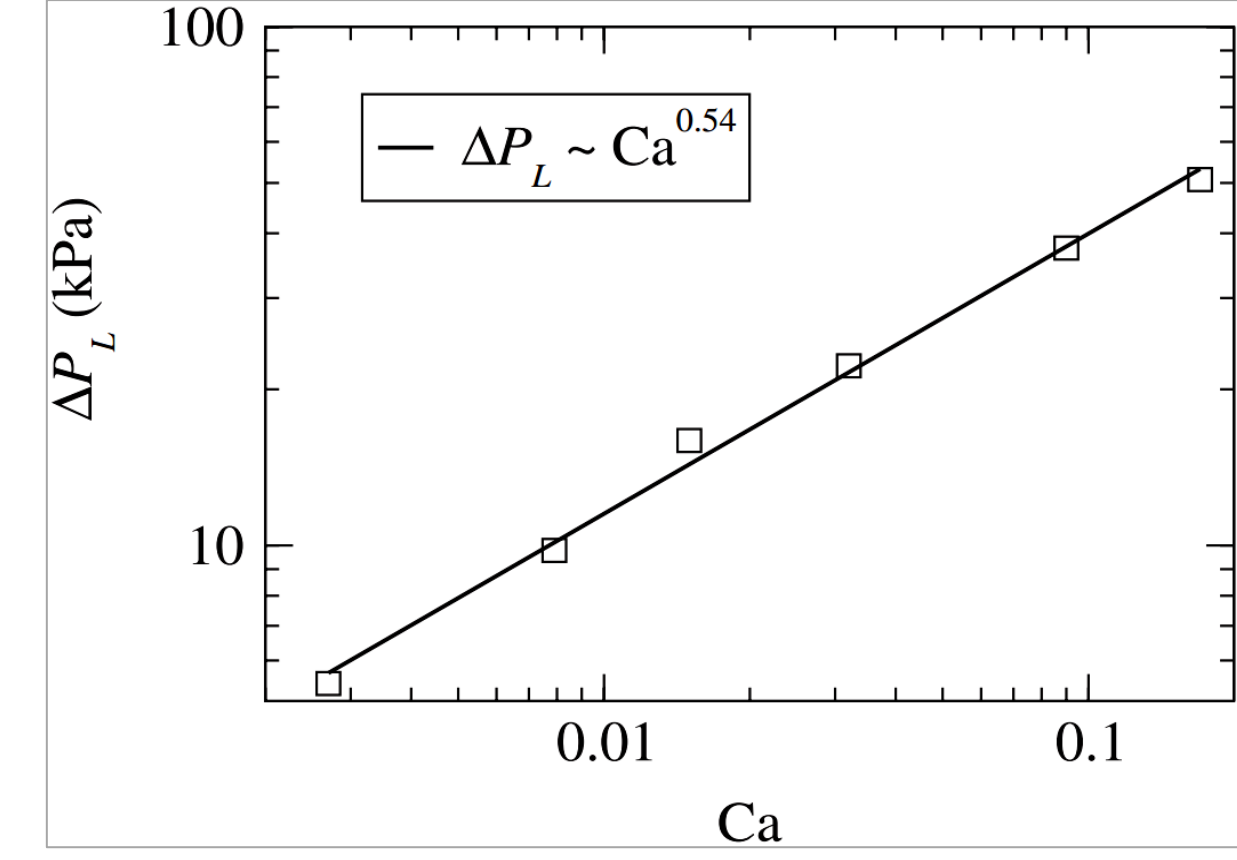
$$\Delta P \sim Q^{0.54}$$

$$Q \sim \Delta P^{0.54}$$

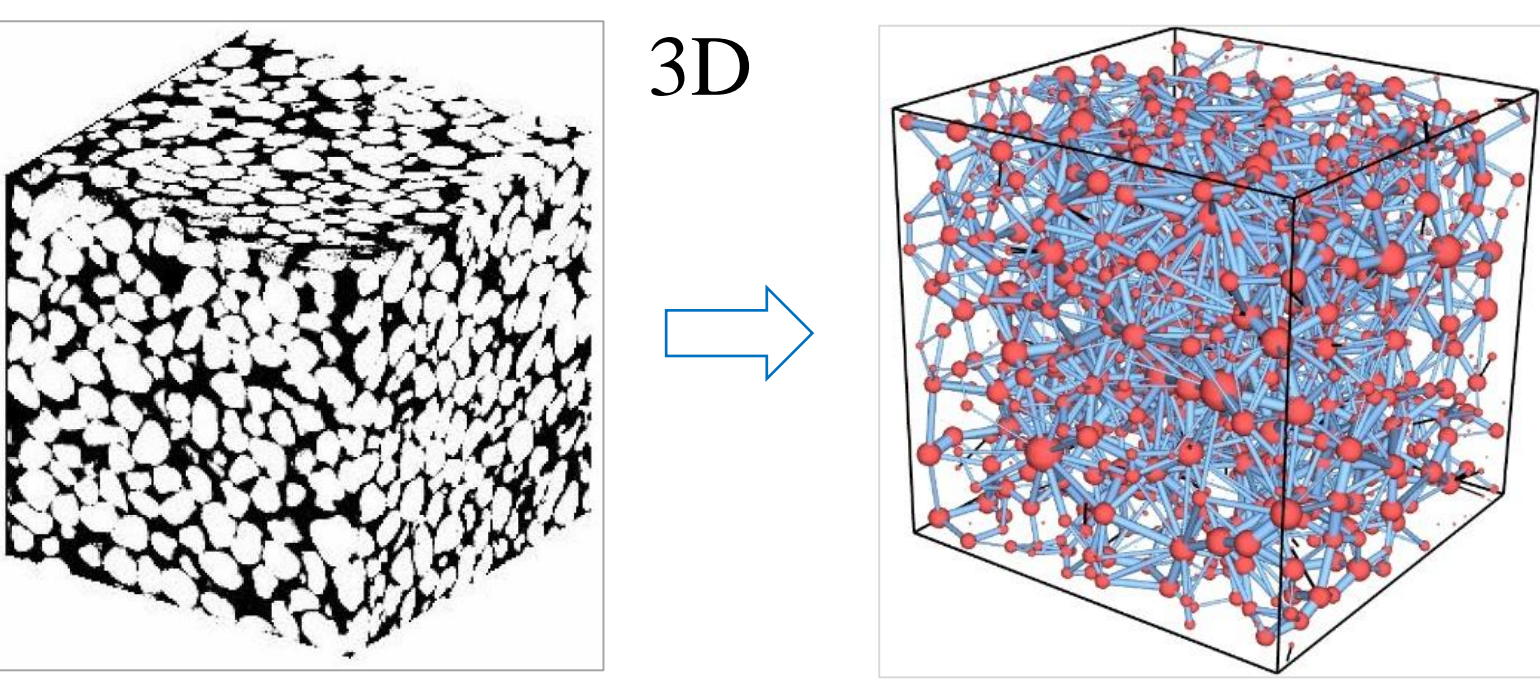
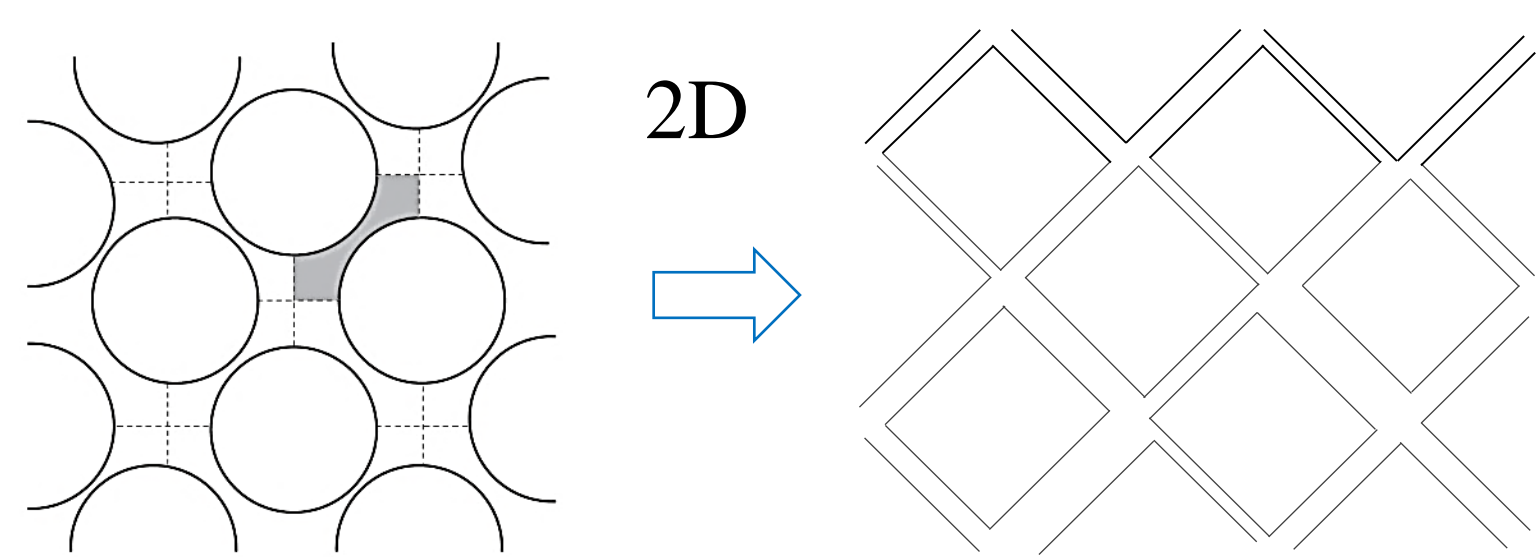
### Transient Behavior



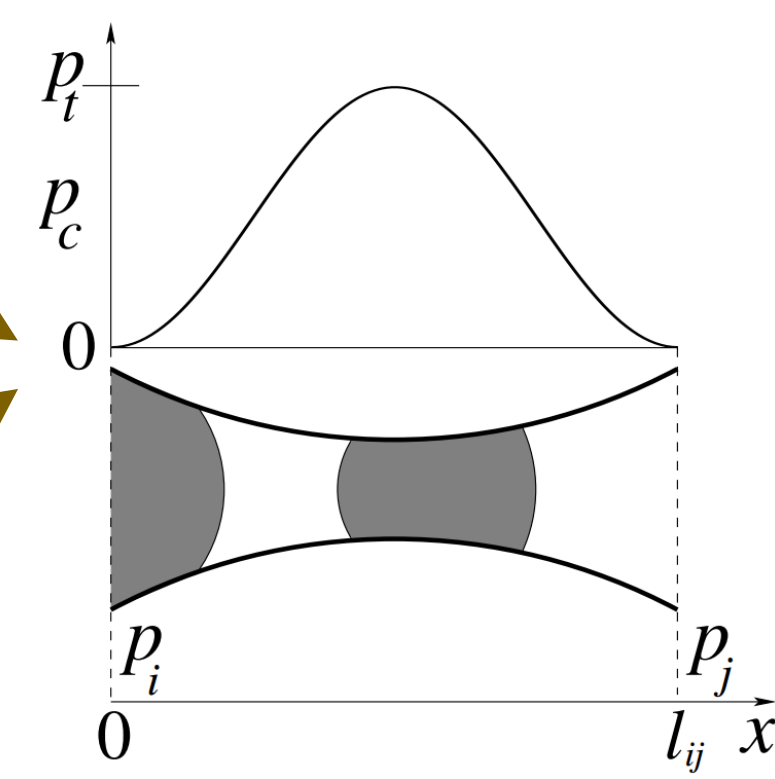
### Steady-state Behavior



## C. Dynamic Pore Network Model [4]



Capillary pressure at an interface: Young-Laplace equation [5]



$$p_c(x) = \frac{2\gamma \cos \vartheta_{ij}}{r_{ij}} \left[ 1 - \cos \left( \frac{2\pi x}{l_{ij}} \right) \right]$$

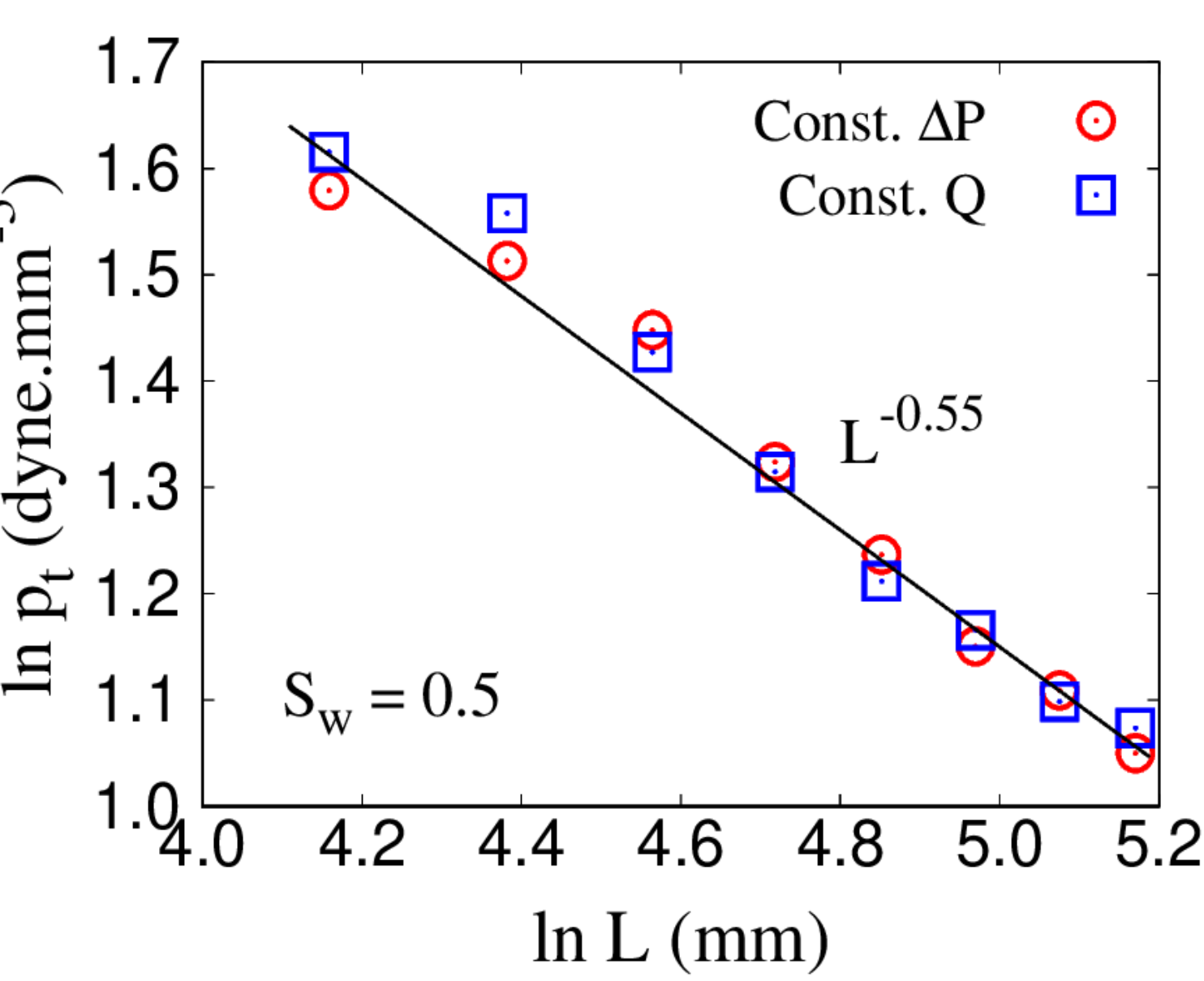
Flow through each pore:  $l_{ij}$ : link length,  $g_{ij}$ : link mobility

Washburn equation [6]

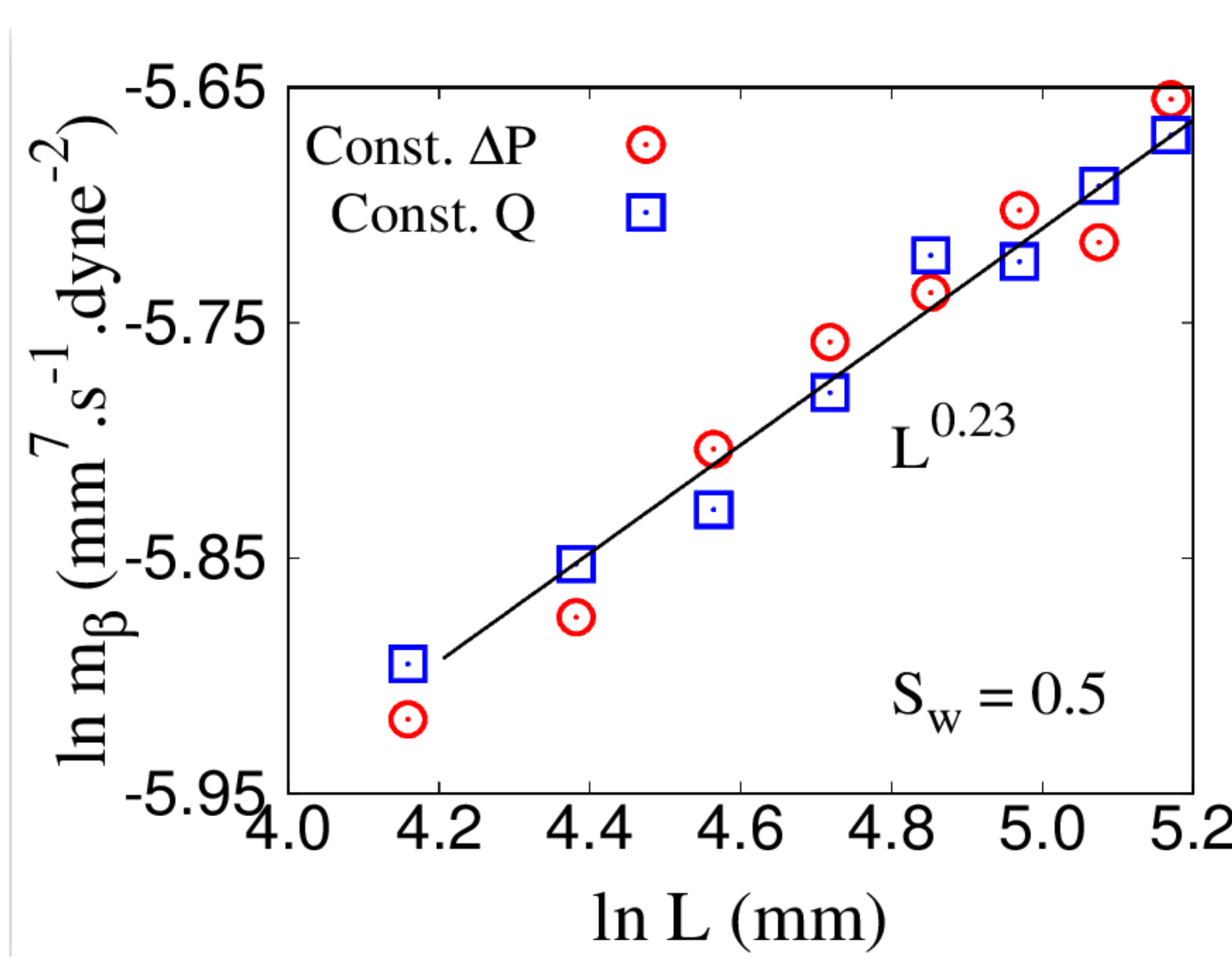
$$q_{ij}(t) = -\frac{g_{ij}}{l_{ij}} \left( \Delta p_{ij} - \sum p_c \right)$$

### Assumptions

- ✓ The fluids are incompressible
- ✓ There is no velocity gradient inside a link. Each link comes with a single velocity/flowrate.



$$p_c \sim L^{-\alpha(S_w)}$$

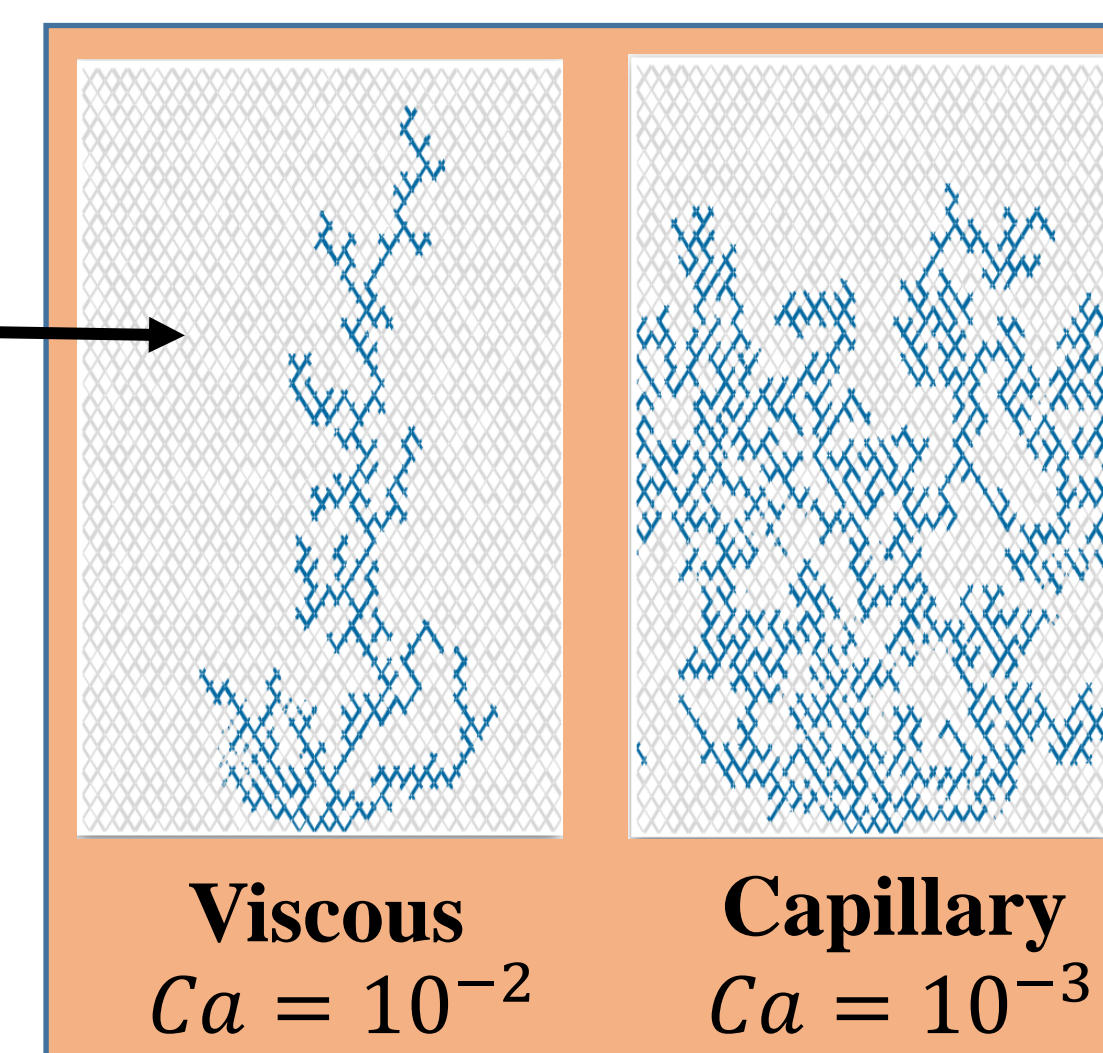
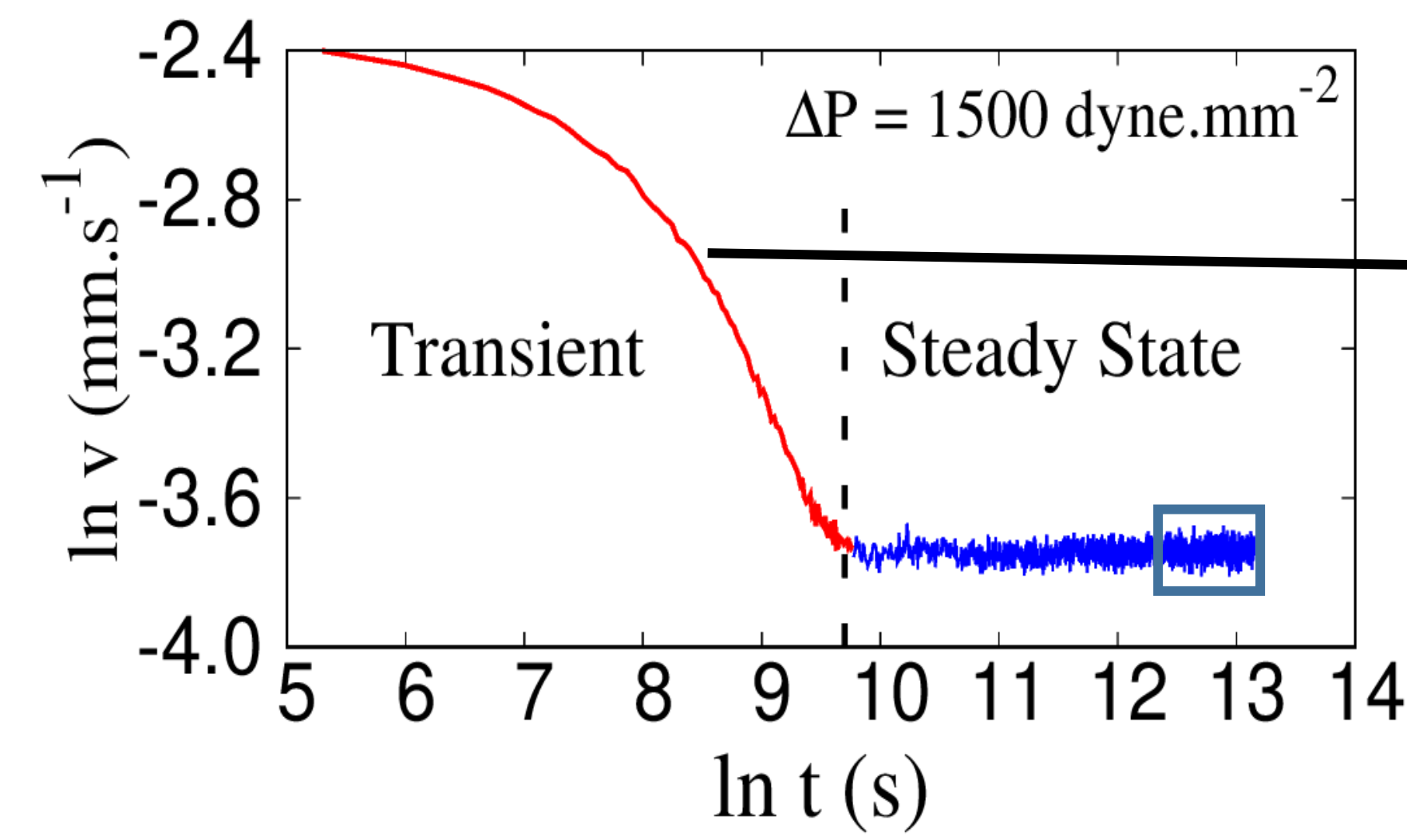


$$m_\beta \sim L^\gamma(S_w)$$

❖ Our numerical results suggest the following observations:

- I. The threshold pressure  $p_t$  decreases in a scale-free manner with system size  $L$ . In the thermodynamic limit we observe zero resistance even if it is a two-phase flow.
- II. The mobility  $m_\beta$  increases in a scale-free manner with  $L$  and reaches infinite in the thermodynamic limit.
- III. Since the 'Darcy line' in case of velocity does not depend on system size, above two factor makes sense only if the non-linear to linear transition point  $p_m$  decreases with increasing  $L$ . This suggest more linear region as size of the system is increased.

## D. Results



Due to the capillary forces there exists a threshold pressure  $p_t$  below which there is no flow.

Just above  $p_t$  the relation between fluid velocity  $v (= Q/A)$  and pressure gradient  $p$  is non-linear due to path opening dynamics [1].

$$Q = -M_\beta \text{sign}(\Delta P) \theta(|\Delta P| - P_t) (|\Delta P| - P_t)^\beta$$

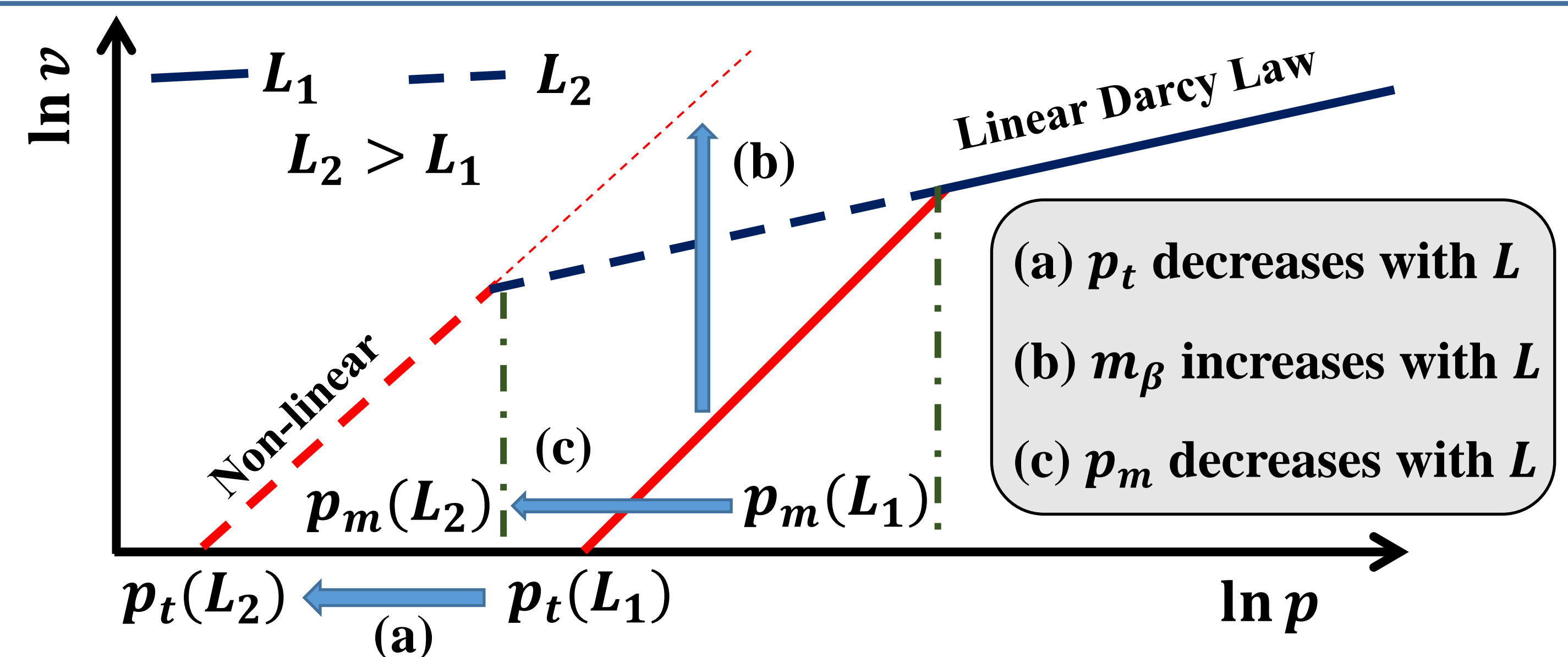
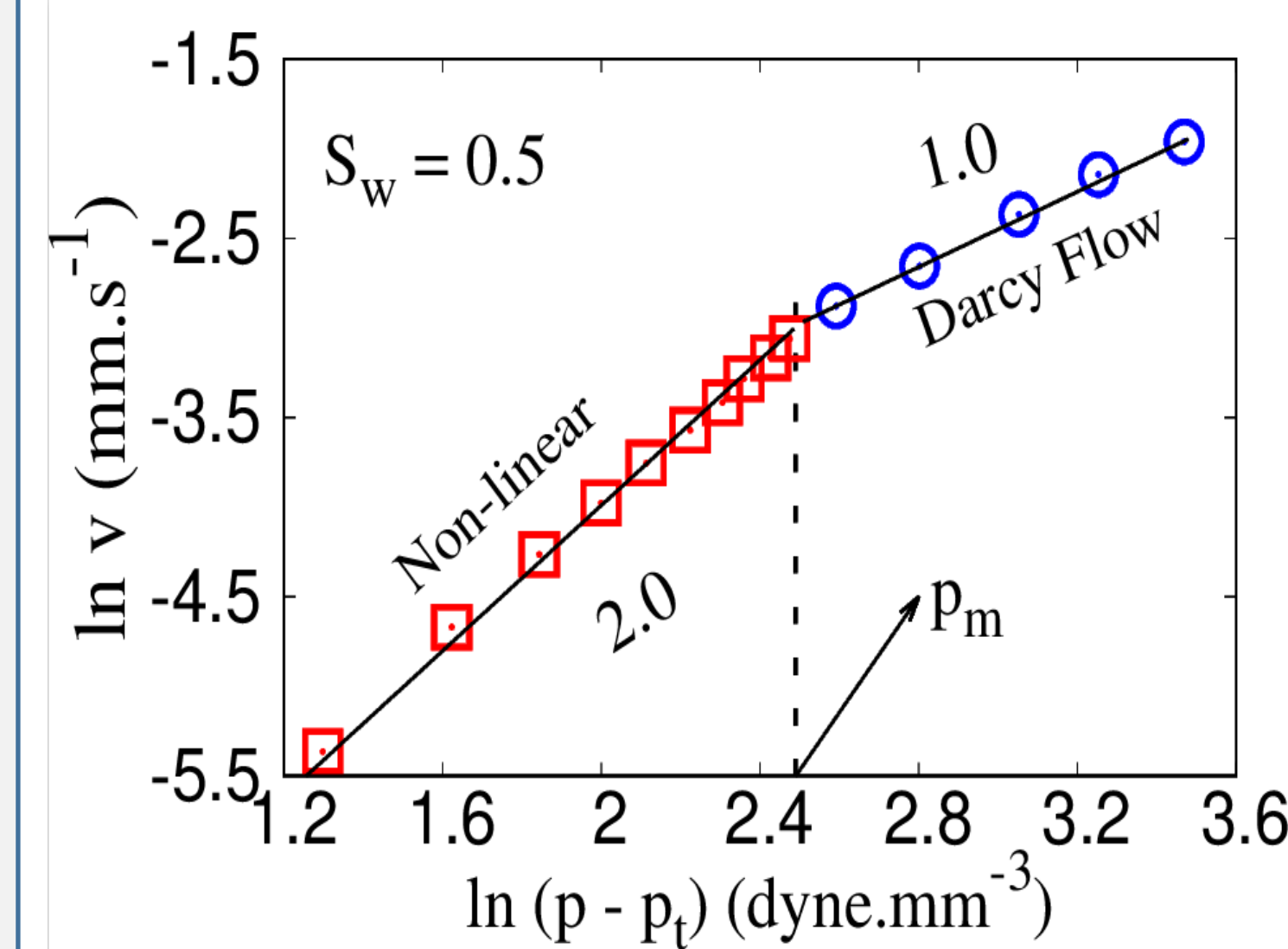
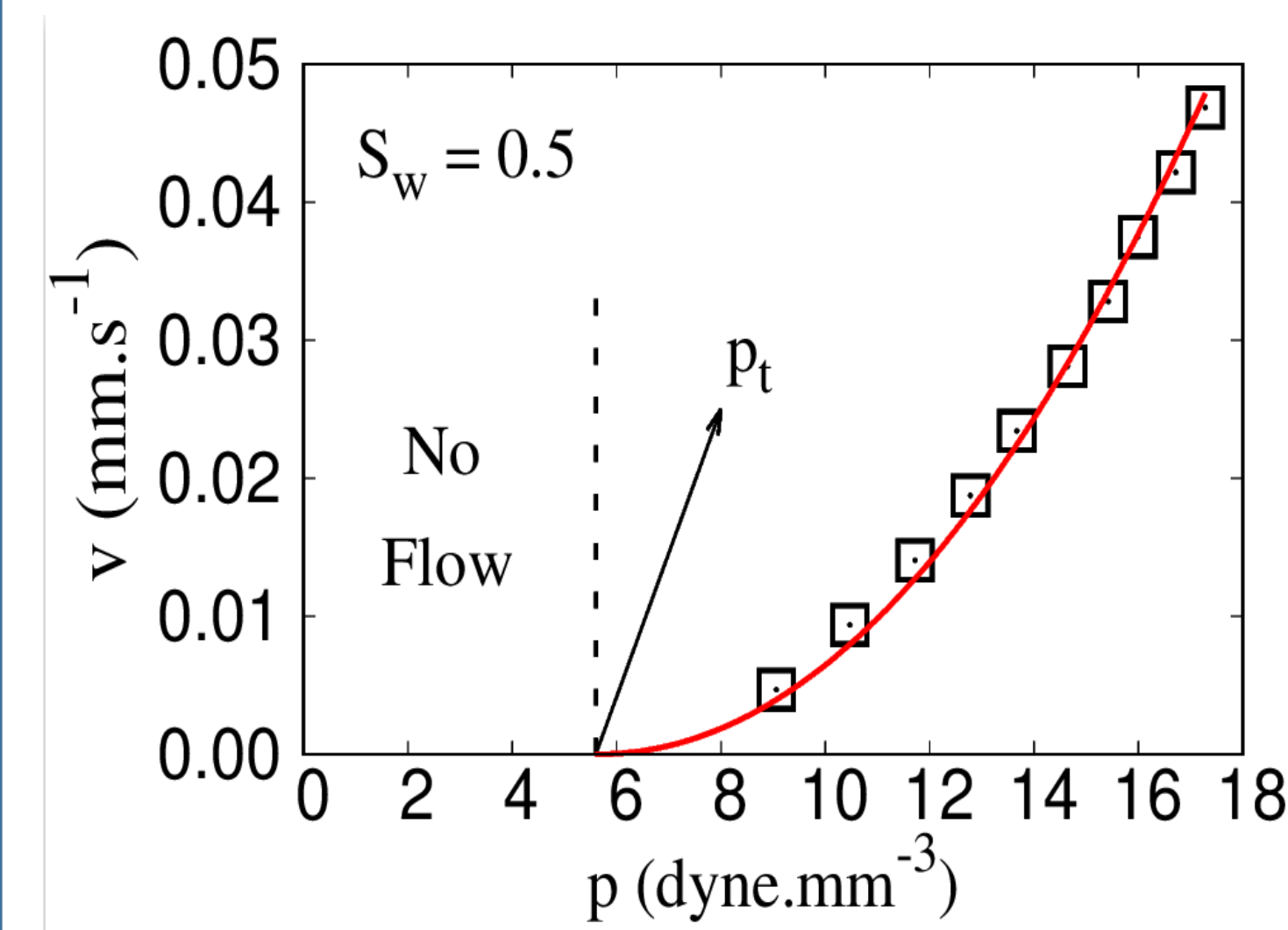
$$v = -m_\beta \text{sign}(p) \theta(|p| - p_t) (|p| - p_t)^\beta$$

Here,  $p_t = P_t/L$ ,  $p = |\Delta P|/L$  and  $m_\beta = M_\beta L^\beta/A$ .

When  $p$  is sufficiently high and all possible paths are open, we enter the Darcy limit [7].

$$Q = -M_d \Delta P \text{ and } v = -m_d p$$

Here,  $p_t = P_t/L$ ,  $p = |\Delta P|/L$  and  $m_\beta = M_\beta L/A$ .



References: [1] Tallakstad et. al, Phys. Rev. Lett. 102, 074505 (2009); [2] Rassi et. al, New. J. Phys. 13, 015007 (2011); [3] Zhang et. al, Geophys. Res. Lett. e2020GL090477 (2021); [4] Sinha et. al, Front. Phys. 8:548497 (2021); [5] Sinha et. al, Phys. Rev. E. 87, 025001 (2013); [6] Washburn, Phys. Rev. 17, 273 (1921); [7] Darcy, H. (1856). Les Fontaines publiques de la ville de Dijon. Paris: Victor Dalmont, 647.